

Study of Longkou Oil Shale Pyrolysis Behavior with Bitumen as the Intermediate

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Abstract. Oil shale as the petroleum alternative is widely distributed in China, the total oil shale resources and potential shale oil resources are estimated at 719.937 billion tons and 47.644 billion tons, respectively. Shale oil and gas can be obtained through the pyrolysis of the oil shale. In order to study of the behavior of the pyrolysis of Longkou oil shale, bitumen as the intermediate products was referenced to the characteristics of the pyrolysis. The result showed that bitumen first output at the pyrolysis temperature of 280 °C and peaked at 340 °C. TGA analysis result of oil shale and bitumen showed that the temperature of bitumen pyrolysis was lower than the oil shale kerogen. The pyrolysis gas of Longkou oil shale could be used to in the production of LNG and LPG.

Introduction

Oil shale is defined as a sedimentary rock that contains solid, combustible organic matter in a mineral matrix. The organic matter, commonly called “kerogen”, is largely insoluble in petroleum solvent. Shale oil is obtained by heating the shale to a temperature of about 500 °C; the pyrolysis of kerogen achieved during heating is generally called “retorting”. Shale oil resembles, but is not identical with crude petroleum[1].

The world's oil shale resources are mainly distributed in the United States, China, Russia, the Congo, Brazil and other places. The world's oil shale resources convert into shale oil is 689.277 billion tons, equivalent to 5.4 times of the world's crude oil [2]. In China, the total oil shale resources and potential shale oil resources are estimated at 719.937 billion tons and 47.644 billion tons, respectively. Oil shale resources are distributed in a wide range, like Fushun, Maoming, Beipiao, Yili and other places. The oil yield of oil shale is between 3.5%-20%, but accounting for 45% and 32% of total oil shale resources and shale oil equivalent is lower than 5%, which are not worthy to be retorted for producing shale oil[3-5].

Oil shale organic matter contains a less amount of bitumen, which is a soluble in common organic solvent. On the other hand, bitumen can also obtained from the pyrolysis of oil shale. The research on group analysis of the Fushun and Maoming oil shale bitumens extracted with chloroform shows that the bitumens are different in characteristics from that from the kerogens pyrolysis. The average molecular weight of bitumen extracted from oil shale is about higher than 1000, it may be regarded as the broken materials form oil shale kerogen, or its homologs, while the average molecular weight of paraffins and aromatics of the bitumen is less than 500, and they may be regarded as the compounds wrapped in the large molecule. In this research, bitumen is regarded as the intermediate during the pyrolysis of oil shale.

Experimental section

Materials and apparatus.

The oil shale sample came from Longkou Shandong province of China, Table 1 and Table 2 shows the ultimate analysis and proximate analysis. The oil content is 15.48wt.% in dry base determined by

the Fischer Assay. The sample was crushed to under 0.15mm particle size and dried 24 hours under 105 degrees Celsius. The pyrolosis device [6, 7] was made up of a reactor placed in an oven to heat the sample. For each test, 30g oil shale sample was loaded into the pyrolosis reactor and heated to the pyrolosis final temperature, the heating rate was 2°C/min, slow heating rate was in order to eliminate the influence of the heat transfer to the pyrolosis, then rapid cooling the reactor to stop the reaction. Bitumen was obtained from soxhlet extraction device to extraction carbocoal.

Analysis methods.

Ultimate analysis of the Longkou oil shale was studied by means of the elemental analyzer , Elementar Analysensysteme GmbH, Germany; Proximate analysis adopt GB/T 212-2001, analysis the moisture, combined water, volatiles, ash and fixed carbon; Thermogravimetric analysis in this research was performed on STA409PC TGA instrument in which the sample mass loss(TG signal), in every experiment, approximately ± 20 mg of samples were heated from room temperature to 600°C at the heating rates of 5, 10, 20, 30and 40°C min⁻¹ under an N₂ atmosphere with a flow rate of 60 mL/min. Experiments were performed twice to ensure repeatability.

Table 1 Ultimate analysis of the Longkou oil shale(%)

Elemental	C	H	O	N	S
Content	32.93	2.71	12.68	0.64	1.27

Table 2 Proximate analysis of the Longkou oil shale(%)

Item	moisture	combined water	volatiles	ash	fixed carbon
Content	1.65	4.28	32.47	44.30	17.3

Results and discussion

The field of pyrolosis products.

Fig 1 shows the field of bitumen, shale oil and carbocoal in different pyrolosis final temperature. The first generation bitumen was at the temperature of 280°C for which content increase to the temperature at 340°C and then decrease, when the temperature was over 440°C, bitumen was no longer produced. With the increase of temperature the yield of carbocoal was decreased, and it was opposite to the field of the shale oil. The adding of bitumen, shale oil and carbocoal was almost 100 percent except of gas and loss.

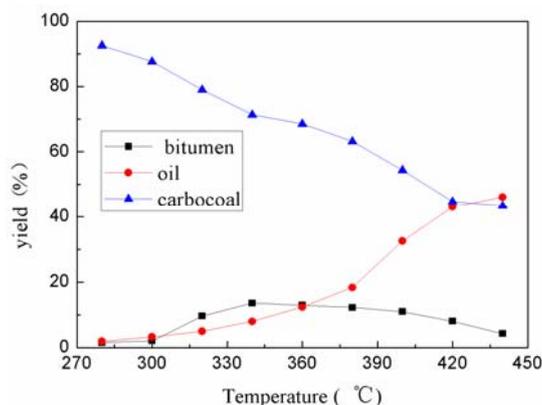


Fig.1 Final temperature vs. the field of bitumen, shale oil, carbocoal

Pyrolosis of oil shale and bitumen.

Fig. 2 shows the weight loss rate of the oil shale samples with respect to temperature during TGA in different heating rates. For TGA, total weight loss includ conversions such as water loss, hydrocarbon generation, and mineral decomposition[8]. Weight loss of 10–30% occurred between 420 and 480°C for TGA experiments. And the weight loss had reached 36% in TGA experiments at 560°C. With the speeding up of the heating rates, the curve of the oil shale pyrolosis moved to the high temperature.

The result of TGA analysis for bitumen pyrolysis weight loss rate at different reaction final temperature 340°C, 360°C and 380°C shows that the weight loss of 10-98% occurred between 300 and 460°C for TGA experiments. With the improvement of the reaction terminal temperature, more content of heavy component was in bitumen, the curve of the oil shale pyrolysis moved to the high temperature with the higher reaction final temperature. Because of the bitumens are different in construction features from the oil shale kerogen, there is more light content in bitumen, the temperature of pyrolysis is lower than the kerogen.

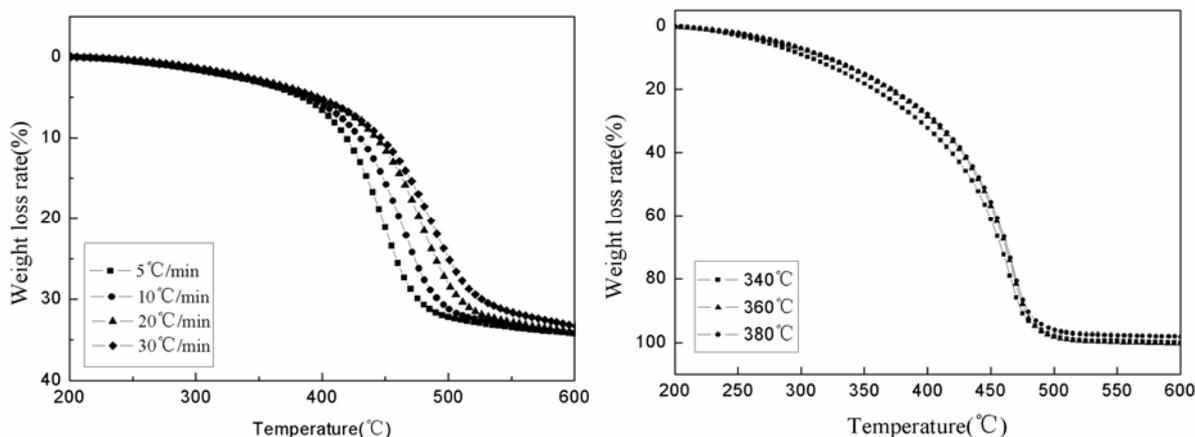


Fig. 2 Weight loss rate vs. temperature for bitumen samples using TGA.

Analysis of pyrolysis gas composition.

Fig.3 shows the pyrolysis gas composition in the reaction temperature of 460°C, because of the geological age of oil shale is young, so nearly 38.8% of the pyrolysis gas is CO₂. Moreover, the content of H₂, CO, CH₄ and C₂H₆ are 22.48%, 10.69% and 7.53, respectively. The calorific value of the Longkou oil shale pyrolysis gas is 617 kJ/mol, so the pyrolysis gas can be used in the production of liquefied natural gas (LNG) and liquefied petroleum gas(LPG).

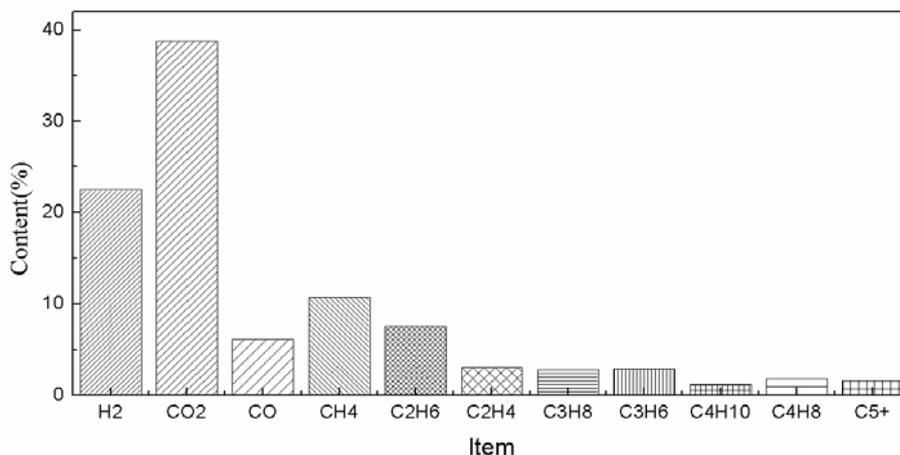


Fig.3 The content of pyrolysis gas composition

Conclusion

In order to get the intermediate products of the oil shale pyrolysis—bitumen, rapid cooling reaction equipment was used to stop the reaction, then using soxhlet extraction device to extraction carbocoal. The result of the experience is the first generation bitumen was at the temperature of 280°C for which content increase to the temperature at 340°C and then decrease, bitumen was no longer produced when the temperature was over 440°C. The experiment get the relationship between the final temperature and the field of oil, carbocoal and bitumen. The interval of pyrolysis temperature of oil shale was 420°C - 550°C and the bitumen was 300°C - 460°C. Compare the weight loss of the oil shale and bitumen through TGA showed that the temperature of bitumen pyrolysis is lower than oil

shale. Over 90% of the composition of pyrolysis gas are CO₂, H₂, CO, CH₄ and C₂H₆, the pyrolysis gas of Longkou oil shale can be used to in the production of LNG and LPG.

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